

# **The Composite Interception Technology of Biochemistry (CITB) for Uranium Pollution Control at the Uranium Tailings**

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# Background

- Great deals of waste rocks, tailing sand and percolate effluent from tailing were produced in the process of uranium mining and metallurgy, which brought the radioactive pollution to groundwater and water bodies.
- The development of groundwater treatment technology of high efficiency and low consumption for uranium and other radioactive contamination, is a major task facing sustainable development of the nuclear industry and the environment protection.



# Introduce of uranium mining & tailings in China

- There are more than 60 mines and 3 uranium mills in China, more than 20 units are underway or would be decommissioning.
- Naturally occurring radioactive material (NORM) due to unregulated activities and artificial radionuclides, mainly resulting from past practice.
- Most of processes of uranium mining are acid in situ leaching, heap leaching and in-situ blasting leaching.
- There are huge waste, high radiation dose and influence widely in uranium mining and metallurgy in China. The radiation dose accounts for 91.5% of entire nuclear fuel circulatory system, and including 80% of uranium tailings' radiation dose. The maximum effective dose of residents is up to 0.65 ~ 1.67 mSv/a by water vapor channels in uranium mining, and 17.5 Sv/a collective effective dose, beyond the criteria specific to existing situations of exposure.



# Introduce of uranium mining & tailings in China

- **Both radioactive pollutants/contaminants and nonradioactive ones exist in situ. Uranium and other heavy metals, as copper, chromium, lead, cadmium, etc. Massive leaching agent, such as concentrated sulfuric acid, sulfate dissolved infusion**

**Uranium and other radioactive or toxic substances: with high ability of migration, long half-life time, large quantity and complex.**



# No 272 Uranium Tailings

Those images come from the largest uranium tailings in Asia



← BACK →



# Introduction of uranium mining & tailings in China

- Usually, control rainwater infiltration by surface covering, combined with shunting of cut-off ditch and drainage. The phenomenon of recurrent acid exists in some decommissioned facilities.
- There are many problems in decommissioning management or treatment in Uranium mining
- Due to radioactive material residues, such as uranium tailings, the ecological environment is or would be threatened by radionuclide in some regions.

**Uranium contamination is one of the core environmental problems in China.**

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## 2 Strategies ,Techniques and processes to control uranium migrate

- The forms of uranium in aqueous, mostly are U(IV) (tetravalent )or U(VI)( **hexavalent** ), other valence state could be neglected. For U(IV), it is easy to form a stable complex with inorganic carbon, and it is difficult to migrate; For U(VI), form of uranyl ion ( $\text{UO}_2^{2+}$ ), it is soluble, easy to migrate.
- **How to** make U(VI) be immobilized and be isolated  
To reduce U(VI) to U(IV) precipitation state by biological, chemical oxidation and reduction
- Separate U(VI) directly by **adsorption (biosorption)** ion-exchange membrane separation
- Reduce (concentration): evaporation



# Techniques for control radioactive waste (water)

- **Comprehensive radioactive waste management**

- **Permanent segregation**

Minimizing the losses to a considerable extent to isolate uranium from biosphere. The main method is disposition, including waste generation, treatment, disposal and predisposal etc.

- **To built tailings for near-surface disposal of low-intermediate level radioactive waste such as uranium tailings, waste rock of uranium mining and metallurgy. (storage or remediation )**

- **To treat radioactive polluted water :**

**Traditional Methods:** Pump and treat, or physical chemical method etc.( ion exchange, evaporation-enrichment method, storage and diffusion; chemical precipitation)

- **Permeable reactive barriers (PRBs) and biological technology**



# The limitation of currently available techniques

- Pump and treat remediation, physical chemical remediation method, are very expensive and difficult to apply or promote in China.
- **Disadvantages of PRBs:** the accumulation and deposition of pollutants will shorten their life cycle while high load, and poor control etc.
- **In PRBs systems, polluted by toxic heavy metals, how long the filler's activity and effectiveness will last? and what will change the environmental conditions and could reactivate immobilized heavy metals?**



# Objective

**to seek the new process and technique with economic, environmental friendly on remediation of water contaminated by radioactive material residues, and control of radionuclide migration**

**to develop high efficiency low consumption, long-term effective uranium pollution control technology, for low-grade uranium resource recovery.**

**Aiming at solving the problem of the accumulation of pollutants in the course of restoration uranium and other radioactive, toxic heavy metals, improve the existing PRBs.**

**Theory & simulation and test methods**

**With biotechnology, environmental chemistry**

Methods

**The composite interception technology of biochemistry (CITB)**

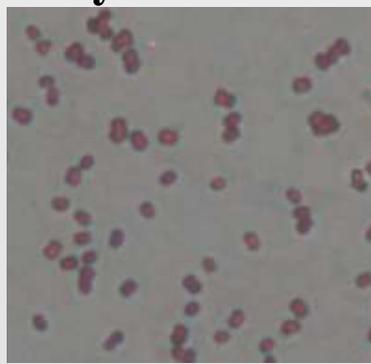


## Study on biomaterial characteristics for processes of CITB

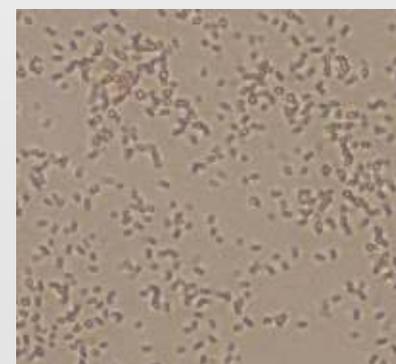
- The **characteristics** of sulfate reducing bacteria (SRB), *Citrobacter sp-* and *Bacillus subtilis*, as well as the characteristics of zero-valent iron reducing uranium from **hexavalent** to tetravalent in the chemical and biological conditions.
- **Advantages of biosorption**
  - There are a growing emphasis on biotechnology on treating uranium-containing wastewater and uranium mining and metallurgy.
  - high efficiency, low operating costs, easy to regenerate biomass & recovery precious metals effectively; adapt to a wide range of pH & temperature; removal mental alternatively with dilute effluents



*Bacillus subtilis*



*Deinococcus radiodurans*



R1



# The adsorption capacity of microorganism to uranium

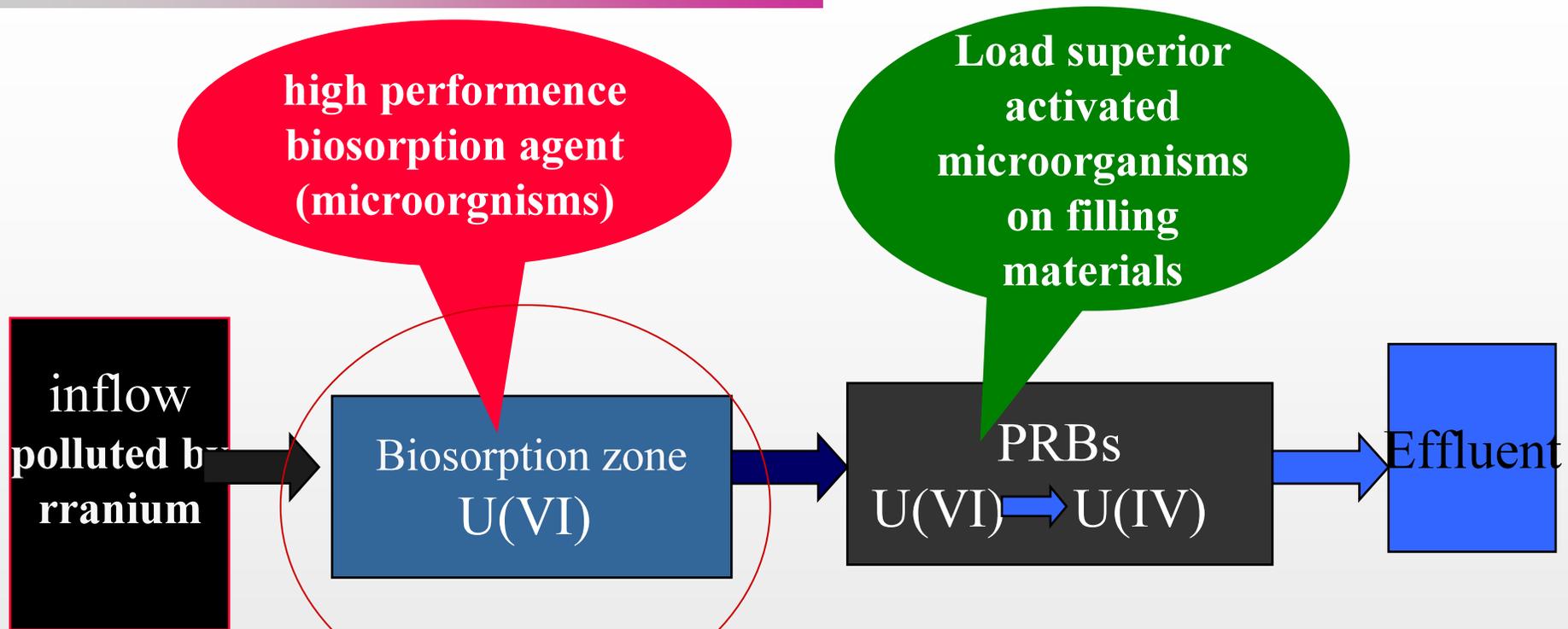
Biosorbents	Biomass	q / (mg·g <sup>-1</sup> )	The order of adsorption capacity of microorganism to uranium
Bacteria	<i>Citrobacter sp-</i> )	9000	Bacteria ≥ actinomycete > fungi > algae
	<i>Bacillus subtilis</i>	615	
	<i>Myxococcus xanthus</i>	571	
actinomycete	<i>Pseudomonas sp-</i>	541	
	<i>Zoogloea ramigeral</i>	400 - 800	
	<i>Streptomyces sp-</i>	440	
<p>The uranium adsorption capacity of <i>Citrobacter sp-</i> was far lower than the former reports of 9000 mg·g<sup>-1</sup> in our studies. Chinese researchers use <i>Rhizopus arrhizus</i> to adsorb uranium, while in overseas using <i>bacillus</i> or <i>pseudomonas</i>.</p>			
algae	<i>Penicillium chrysogenum</i>	170	
	<i>Saccharomyces cerevisiae</i>	172	
	<i>Sargassum fulitans</i>	560	
	<i>Anabaena azollae</i>	1.6	

400-9 000

1.6-560



# 3 The Characteristics of the CITB



At the first zone, microorganism immersed into it, most of uranium is adsorbed by died bacterial mass, the efficiency of adsorption to uranium would have been improved by pretreatment of bacterial mass; at the second zone (PRBs with engineering strain), the uranium is precipitated by biochemical reaction or adsorbed by microorganism. The metal which had been adsorbed could be desorbed for recovery. Through biological adsorption, and PRBs and SRB+ZVI coordination, the rest concentration of effluent is less than effluent-quality standard of China.



# 3 The Characteristics of the CITB

- In front of PRBs, There is a biosorption zone with excellent sorption materials and suitable sorption environment; inducing SRB to PRB, optimizing fillings such as ZVI and fluor, developing the synergy of SRB and ZVI, the composite interception technology of biochemistry for uranium pollution control at the uranium tailings—efficient compound PRB was put forward.
- The uranium pollution control and the recovery of low-grade uranium resources would be achieved, taking full advantages of the synergy of inorganic materials and biomaterials, for which the uranium in effluent was efficiently absorbed in forepart, and then adjusting pH to 5. The experimental results proved that it is efficient to control uranium pollution.



## 4 The Test for CITB

- Optimizing **test**, evaluate the functional biomaterials
- **Biosorption agents for absorption zone:** adsorption properties of superior microorganisms and its influencing factors (*Citrobacter sp-*, *Bacillus subtilis*, *Saccharomyces cerevisiae*, )
- Filling materials and strains for PRBs: SBR and others, reducing agent, the capability of ZVI, fluor, hematite etc.
- Mechanism of removing uranium cooperatively by *Sulfate reducing bacterial & ZVI*.
- Environmentally-friendly catalyst for biochemical reaction catalyst: *Deinococcus radiodurans*. **SRB-1 is a kind of artificial breeding engineering stains**
- Construction strategy and functional analysis of *Deinococcus radiodurans*
- An plot experiment of uranium control in some solution mining uranium
- To investigate the effect factors condition for removal rates of U (VI), such as, pH, initial concentration of uranium, **coexisting ions**, reaction time by ZVI and hematite.
- The reaction kinetics and thermodynamics about the removal of uranium (VI) from wastewater by ZVI and hematite.



## 4 The results of test for the process of CITB

- The experiment indicated that the biosorption plays a primary role in the forepart of the efficient compound PRB, and SRB-1 catalyses and reduces uranium from **hexavalent** to tetravalent through ZVI after that.
- It is the key to control pH properly that prevent uranium and other metals remigration from causing secondary pollution. Also it is crucial for performance of engineering processing, through optimizing adsorption process, controlling pH and the concentration of heavy metal ions such as copper, and strictly controlling the effect of nitrate ion to the process.
- The steady and preponderant SRB-1, *Citrobacter sp-* and *Bacillus subtilis* were obtained through screening test. The mechanisms and immobilization of biomass were also studied and successfully applied in industrial process.



## Removal of U(VI) from wastewater by ZVI and hematite

**Iron is an active metal with reducibility, and was an efficiency filling material. Iron powder can react with heavy metals and some organics, and make them precipitate. It can reduce heavy metal ions or compounds with stronger oxidization and some organics . In aqueous solution , iron and other elements could easily form primary battery:**

**anodic reaction:  $\text{Fe} - 2\text{e} \rightarrow \text{Fe}^{2+}$   $E_0(\text{Fe}^{2+}/\text{Fe}) = -0.440 \text{ V}$**

**cathodic reaction:  $2\text{H}^+ + 2\text{e} \rightarrow 2[\text{H}] \rightarrow \text{H}_2 \uparrow$  ,  $E_0(\text{H}^+/\text{H}_2) = 0.00 \text{ V}$**

**when oxygen dissolved in water:**

**$\text{O}_2 + 2\text{H}_2\text{O} + 4\text{e} \rightarrow 4\text{OH}^-$   $E_0(\text{O}_2/\text{OH}^-) = 0.40 \text{ V}$**

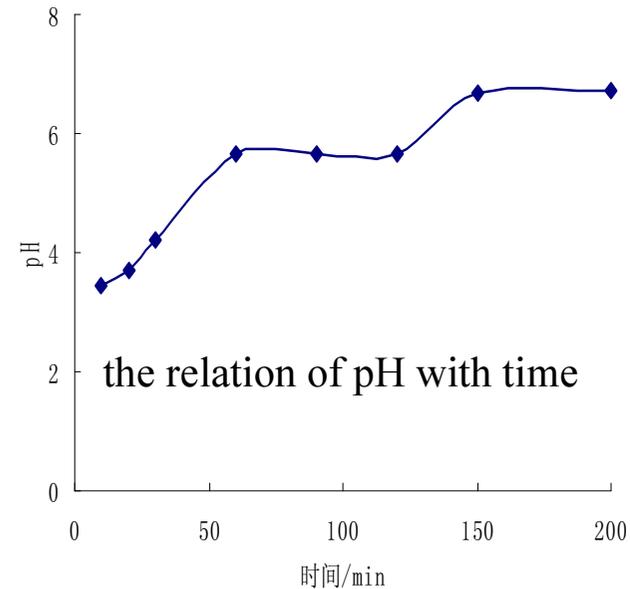
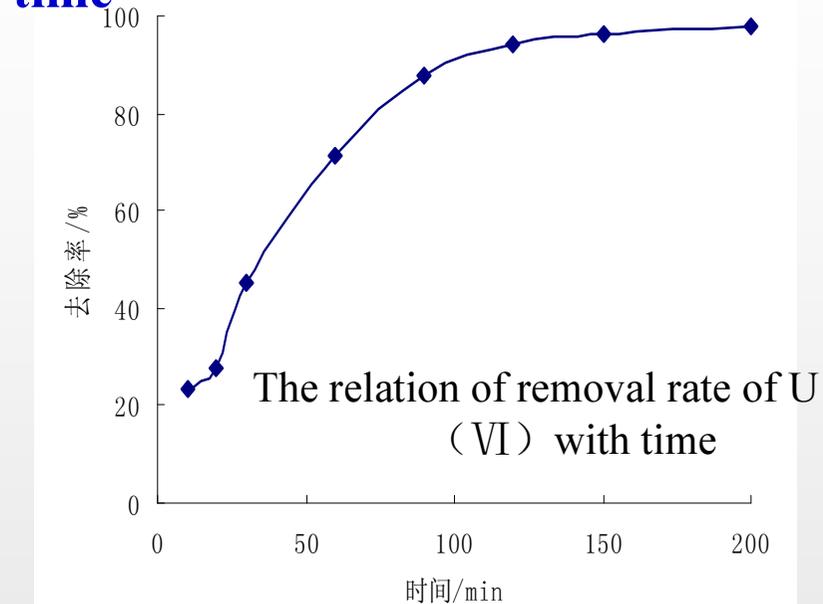
**The oxides of iron, especially hematite and goethite are the common components of soil, sediments and water, there are large sp. surface area and strong adsorption.**

**ZVI 's good nature material for treating heavy metals in wastewater, it be selected to build large scales of PRBs for remediation of land and water contaminated by waste material residues.**



# Results and Analysis

## Efficiency test of the removal of U(VI) in solution by ZVI with reaction time

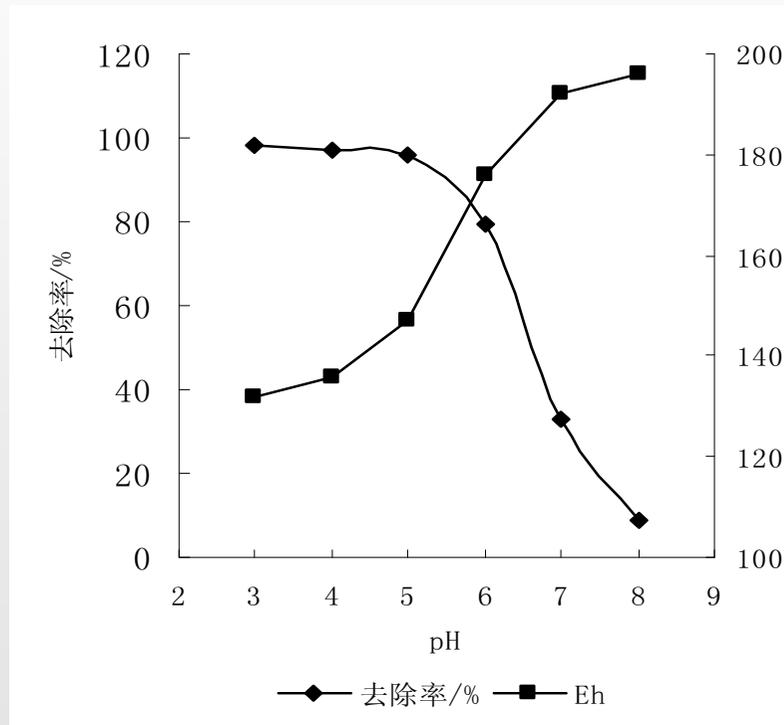


**At the initial stage, the removal rate reached 88% when at 90min, when 200min, it reached 98.1%. Because of the higher concentration of U(VI), the sediments adhered the iron surface were relatively less than to make the reaction of reduction precipitation of U(VI) quicker. With the reaction going on, pH increased, iron oxides, the corrosive products of ZVI would attach with the iron surface, holding back the reaction. In the reduction precipitation of U(VI) by ZVI, amounts of  $H^+$  in the related electrochemical reaction were consumed, the concentration of  $H^+$  decreased, pH increased.**



# Removal of U(VI) from wastewater by adsorption of ZVI

## Effect of removal rate by initial pH



As the initial pH increased, the removal rate of U (VI) decreased, when pH was over 5, it decreased rapidly. At acid condition, uranium existed as  $UO_2^{2+}$  which was reduced by ZVI suitable, when near neutral and alkaline, it existed as other complexions, these complexions inhibited the reduction of uranium, oxidation-reduction potential increasing with pH increasing, illustrated that the decreased

Without organisms to catalyze, acidic (weakly acidic) conditions were helpful for reduction of uranium by ZVI.

# Removal of U(VI) from wastewater by adsorption of ZVI

Effect of the removal rates of U (VI) by the amount of the iron powder

The removal rates of U(VI) were not improved significantly excessive iron powder

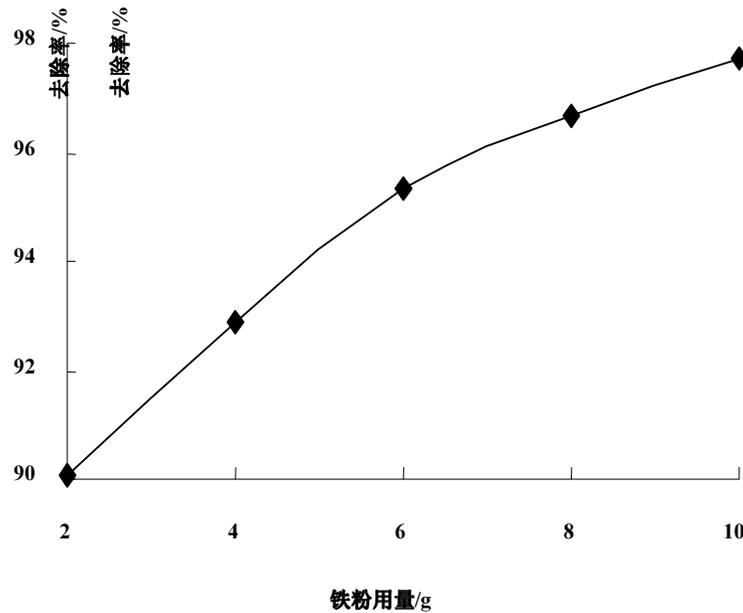


Fig.4 Effect of removal of U(VI) from aqueous solution by adsorption of ZVI

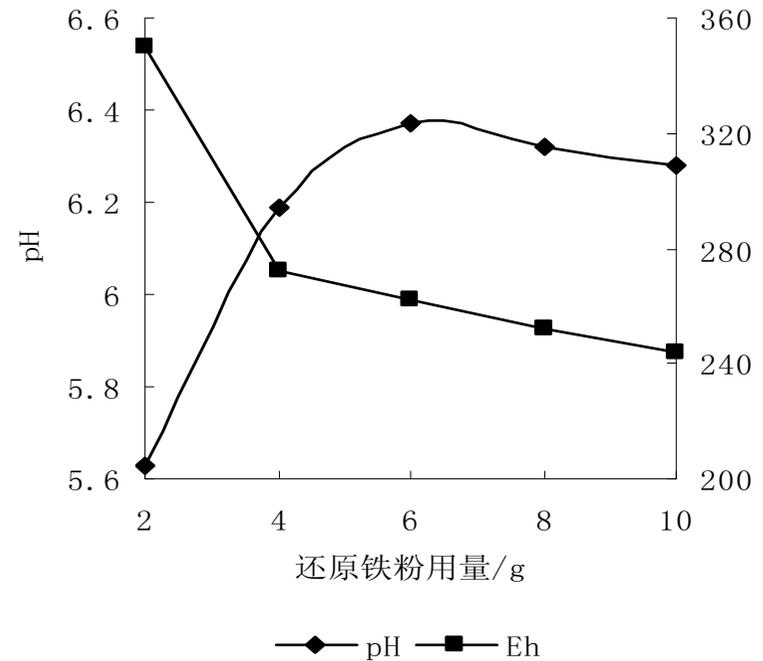


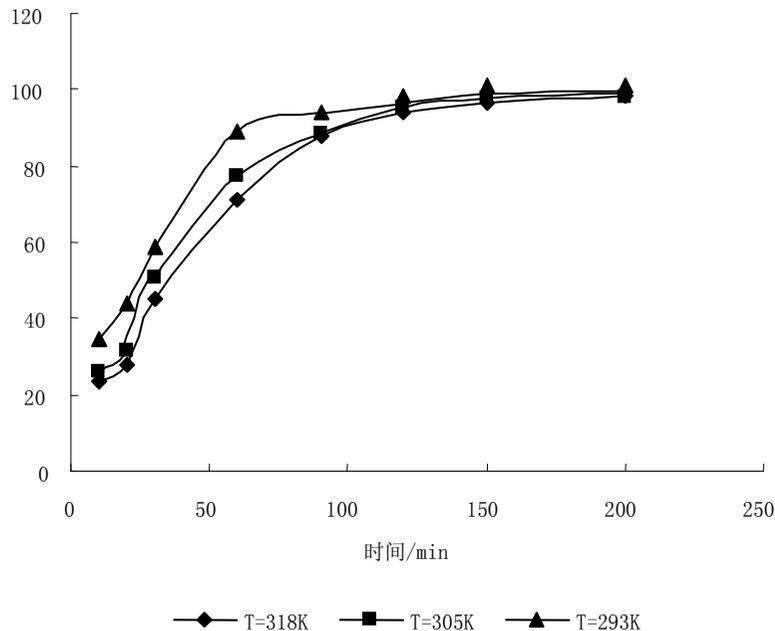
Fig.5 Relation of pH、Eh and the amount of reduced iron powder



# The test of hematite and ZVI removing the U(VI) in wastewater

## Relation of the U(VI) removal and time with the different temperature

## Analysis of the reaction dynamics



The influence of temperature on reaction rate

shows the degree of influence of the mass

transfer on the reaction dynamics. For the typical

mass transfer reaction dynamics, Diffusion is the

limiting factor, activation energy of the reaction

may be small; for the dynamics controlled by

chemical reaction, the influence of temperature

on reaction rate is not too big.

**From the above graph, the degree of change is not so sharp within the different temperature, the reaction of the U(VI) and ZVI is controlled by the chemical reaction.**



## the reaction dynamics

The table below is from the the result of the uranium concentration from the test along with the changing time and concentration calculation formula . And dynamics constant and correlation coefficient are calculated by the regression .

Table 1:  $C_t$ ,  $C_t$ ,  $-\ln(C_t/C_0)$  and  $-(1/C_0 - 1/C_t)$  along with the changing time

time/min	10	20	30	60	90	120	150	200
$-C_t$	-15.34	-14.49	-10.99	-5.74	-2.40	-1.23	-0.76	-0.38
$-\ln(C_t/C_0)$	-2.73	-2.67	-2.4	-1.75	-0.68	-0.21	0.27	0.97
$-(1/C_0 - 1/C_t)$								

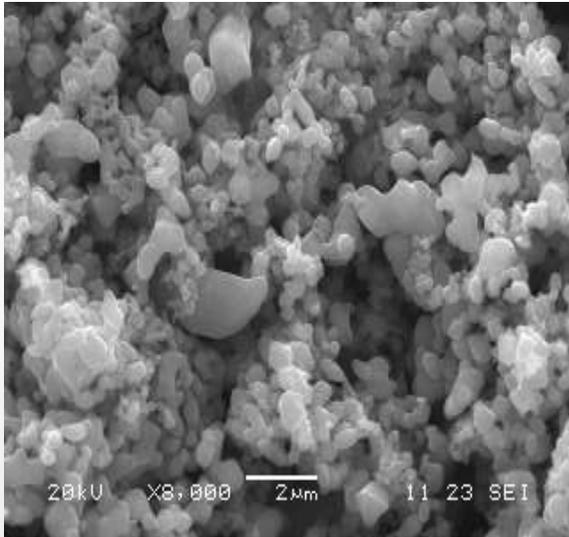
In the scope of the initial concentration, the zero-valent iron to remove U (VI) in the water is the first reaction , whose correlation coefficient is 0.9863.

Table 2: correlation coefficient for different instances

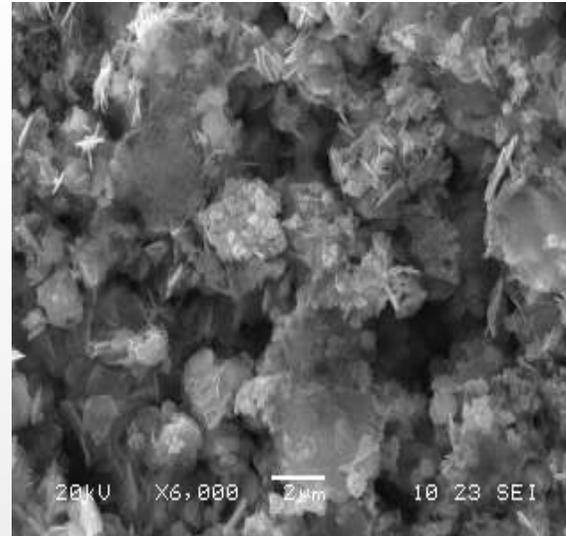
Reaction series	Zero series	first series second series	first series second series
$R^2$	0.7897	0.9863	0.9788



# Electronical microscope analysis of ZVI to remove U (VI)



before electronical microscope analysis



after electronical microscope analysis

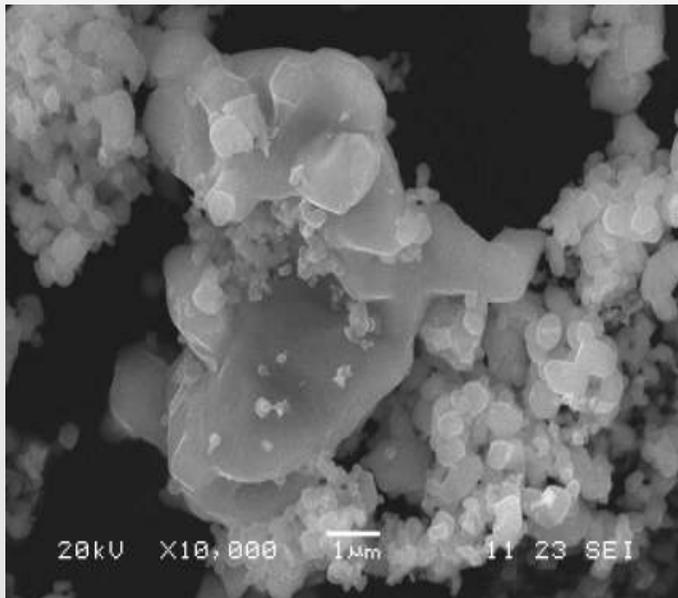
The surface of iron powder is smoothly, not centralized and no lamellar crystal at the reacting of beginning. The result is opposite after the reaction has finished, arborescent surface is surrounded, and more thick. It indicated that the surface iron is eroded, new substance deposited on the surface of the reduced iron, blocking the reactant connecting active sites of ZVI, to reduce its activity.



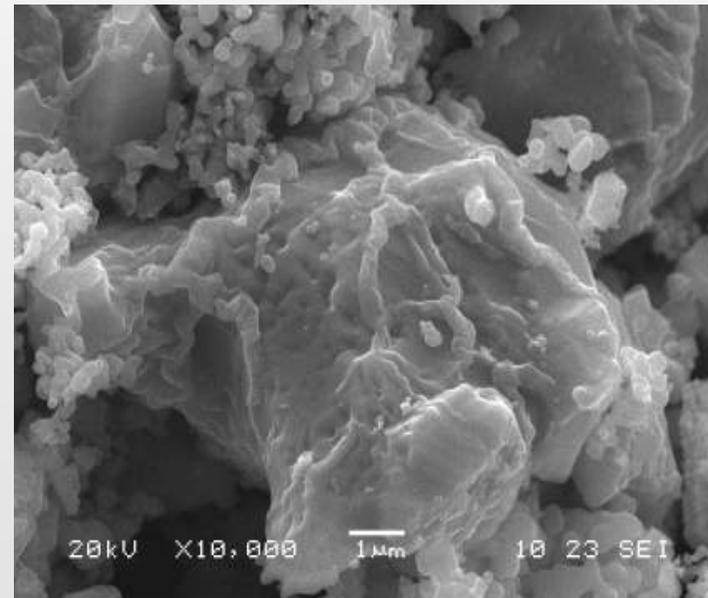
# Mechanism analysis

**It was obviously that hexagonal crystals and quartet crystals coexisted and it is abundant. The hexagonal crystals are  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub>, the main component of hematite and square crystals are magnetic hematite (Fe<sub>3</sub>O<sub>4</sub>), the secondly component.**

**ESEM of hematite having adsorpted U(VI)**



**Before adsorption**

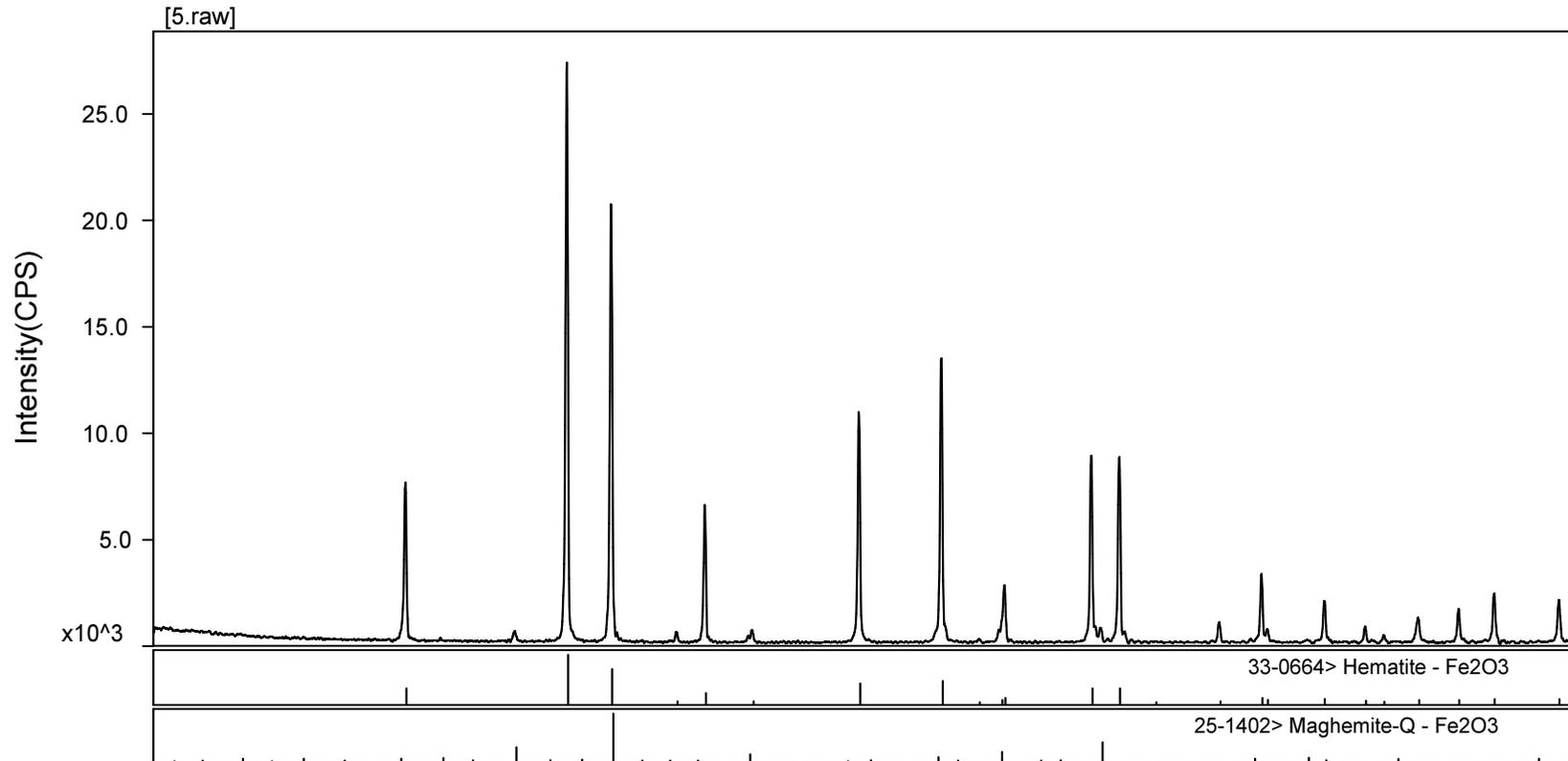


**After adsorption**



# Mechanism analysis

## X-ray diffraction patterns of hematite



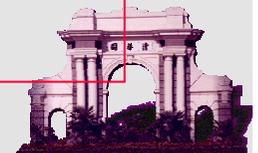
It can't be seen the diffraction peaks of crystals formed by uranium. It may be explained that the complex formed by U(VI) in neuter solution didn't form crystal lattice after adsorption to the surface of hematite with the function of electrostatic force.



**ZVI is mainly precipitated by the electrochemical corrosion solution to restore the U (VI), and reduced U (VI) to U (IV) fixing. Electrochemical reaction of a new generation of [H], Fe<sup>2+</sup>, OH have a strong reduction, etc., and can damage the structure of UO<sub>2</sub><sup>2+</sup> to make it into a stable U (IV) , Iron hydroxide generated and its adsorption of U (VI) of sediment play a very important role. by the flocculation precipitation of iron corrosion products .**

**To use ZVI alone, the acidic conditions is U (VI) to remove the better, with the pH increase in, U (VI) to reduce the removal rate. When the pH = 3, the removal rate can reach 98.1%; when pH > 5, the removal rate of a sharp decline, that zero-valent iron to remove U (VI) in response to low pH conditions easier. Excess iron did not significantly improve U (VI) removal rate.**

- **X-ray powder diffractometer (D/MAX -2400)**
- **X-ray fluorescence spectrometer (XRF- 1500)**
- **Scanning electron microscope (LEO1450VP)**



## The Efficiency and Mechanism on Reduction of U (VI) by SRB

- Under anaerobic conditions, the characteristics of SRB applied to reduce U(VI) were investigated under different temperature, the concentration of U(VI), pH, and the coexisting ions.
- The results showed that the optimum reduction conditions was the temperature of 35°C, pH 7.0 and concentration of U (VI) 25 mg·L<sup>-1</sup>.
- The maximum reduction capacity of SRB was 179.1 mg·g<sup>-1</sup>. Mo(VI) or Ca<sup>2+</sup> did not affect SRB on the reduction process of U(VI) under the concentration less than 5 g·L<sup>-1</sup>, but they strongly inhibit the process under the concentration more than 20 g·L<sup>-1</sup>.
- The main inhibition of Mo(VI) was physiological inhibition and the inhibition of Ca<sup>2+</sup> was competitive inhibition through the stable complex formation, Ca-UO<sub>2</sub>-CO<sub>3</sub>. The results also showed that lag phase did not appear on the concentration of Ca<sup>2+</sup> less than 5 g·L<sup>-1</sup>, but the lag phase of 24 hours appeared on the concentration of Ca<sup>2+</sup> more than 20 g·L<sup>-1</sup>.



**The effect of pH is big to hematite remove U (VI) ,and the removal rate proves in positive correlation with pH , Under the acid conditions removal rate is quite low and only 14.8% at pH=3,while reach 89.1% at pH=8; Coexistence ion such as  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$  didn't affect the adsorption of uranium by hematite significantly when its concentration is about  $10^{-3}\text{mol}\cdot\text{L}^{-1}$ .**

**ESEM analysis the component of hematite powder indicated that the hexagonal crystals are  $\alpha\text{-Fe}_2\text{O}_3$  and square crystals are magnetic hematite ( $\text{Fe}_3\text{O}_4$ ).The X-ray diffraction spectrometry test results of hematite after response can't be seen the diffraction peaks of crystals formed by uranium. X-ray fluorescence spectrometry analysis showed that the content of uranium is equal to that of uranium in adsorption.**

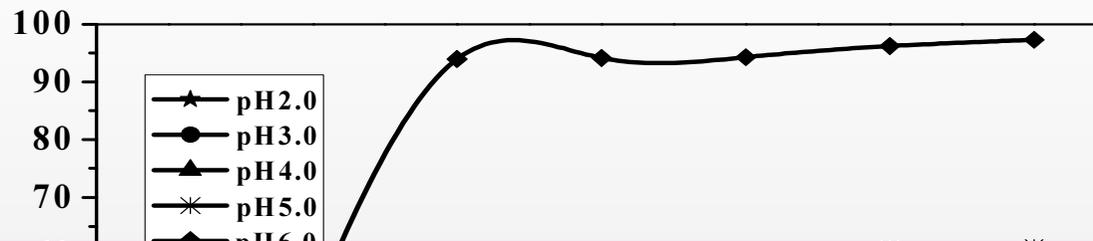
**The pseudo-second-order kinetic model is appropriate to describe the adsorption process of U(VI) by hematite, and correlation coefficient is 0.9959. The max adsorption capacity is  $3.54\text{ mg}\cdot\text{g}^{-1}$  at  $T=293\text{K}$ . The adsorption of U(VI) by hematite fit for Langmuir equation.**

**For the mixed pollutants, the repairing effect will be better by the filling material of mix material. Such as mixed hydroxyl ferric oxide, zeolite and other materials. The mixed strain to U (VI) have highly effective.**



# SRB to repair uranium wastewater pollution

## The initial pH value of U (VI) to restore the biological effect



SRB of U (VI) reduction capacity and pH values are related

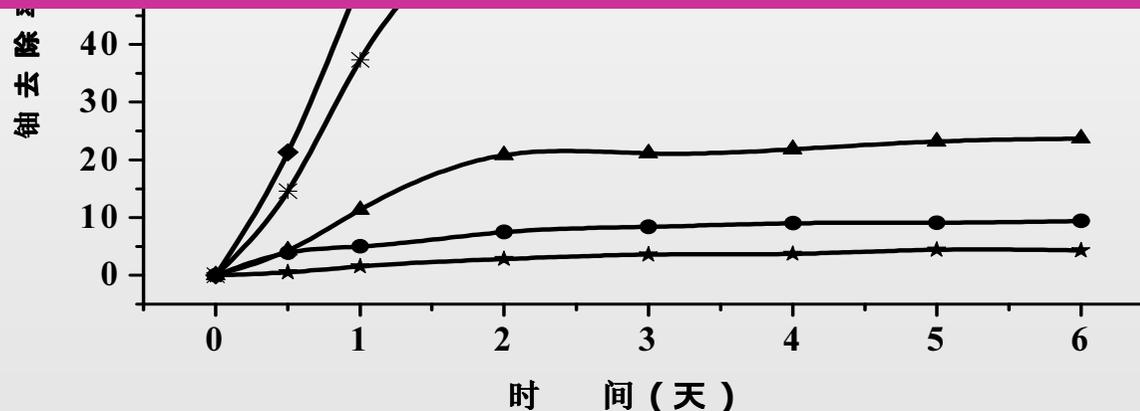


fig8 Different pH conditions, the impact of removal of uranium

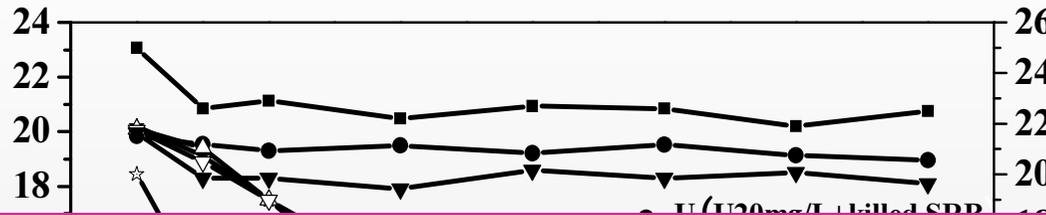
U (VI) initial concentration 20mg / L, when the initial pH value of 2.0 and 3.0, the experimental U

sedimentation rate after less than 10%; the rise in pH value, SRB of U (VI) reduction capacity. The initial pH value rose to 6.0 from 2.0 hours, U (VI) reduction rate from 4.3% to 99.2%.



# SRB to repair uranium wastewater pollution

the results of SRB at co-existence of heavy metal ions to restore the sediment U (VI)



SRB death does not have to restore the ability of U-rich, high concentrations of Zn (II) will precipitate uranium

Death does not have to restore the ability of SRB, high concentrations of Zn (II) so that bio-precipitation of uranium and sulfate-reducing dynamic completely inhibited. Zn (II) in low concentration has little effect



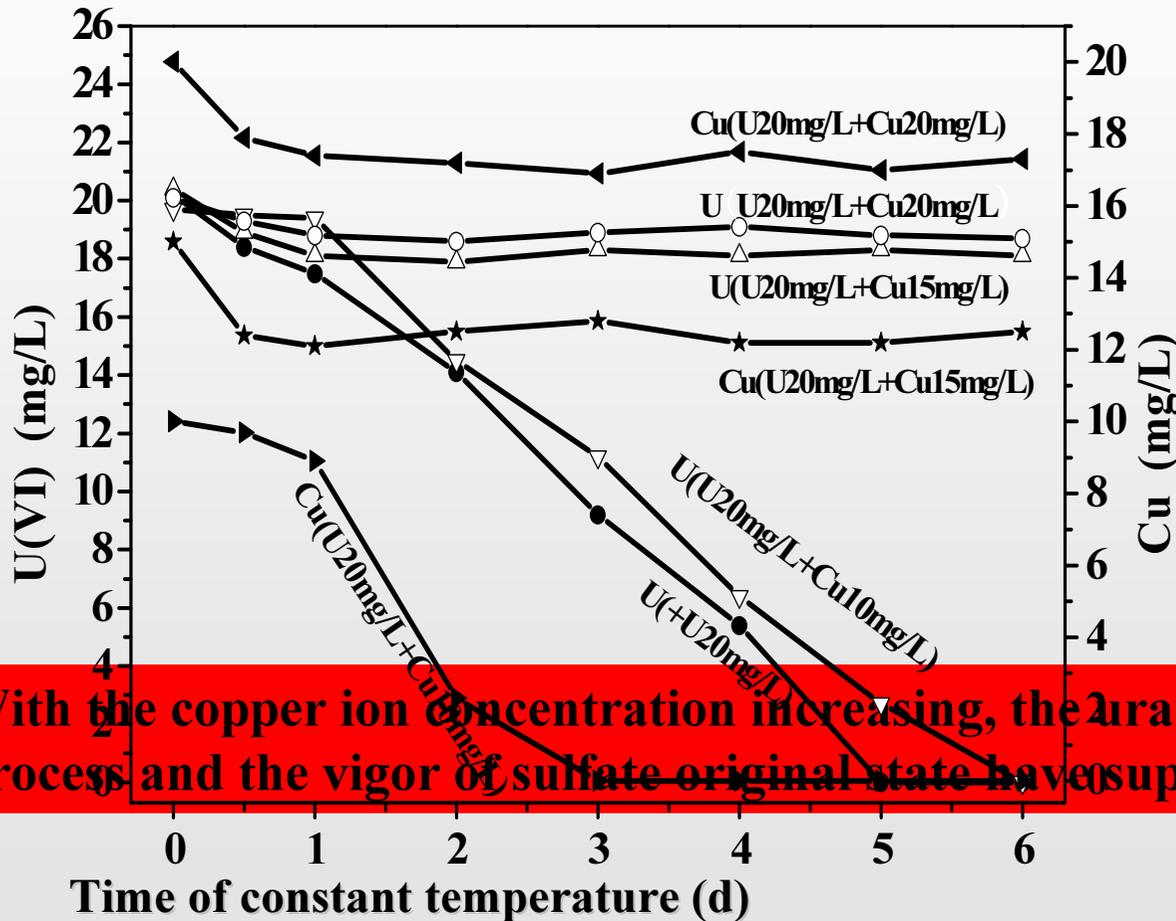
metals). Zn (II) in the 0 ~ 20mg / L of the low concentration range of bio-precipitation process of uranium has little effect; low concentration of Zn (II) was completely removed in the 2d maintained a vigorous show that sulfate-reducing vitality.

fig9 Different concentrations of Zn (II) co-exist on the impact of sedimentation U



# The experiment of sulfidogenic bacteria repair the waste water of uranium

## Effect of different concentration Cu(II) coexistence



Initial concentration of Cu(II) was 10mg/L, that respond 6d with black group, U(VI) may completely precipitate gets down, but it presented the 1d slow time, and produced the H<sub>2</sub>S gas, the black precipitate of bottle base was UO<sub>2</sub>+CuS/UO<sub>2</sub>, With the copper ion concentration increasing, the uranium biogenic sediment process and the vigor of sulfate original state have

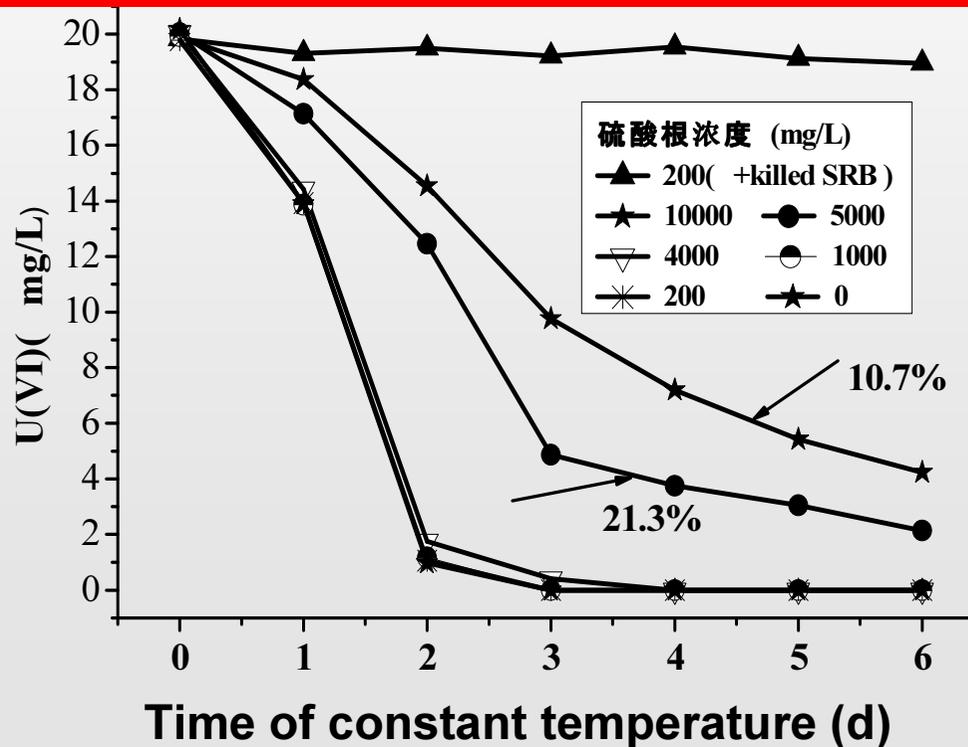
With the copper ion concentration increasing, the uranium biogenic sediment process and the vigor of sulfate original state have suppressed



# The experiment results of sulfidogenic bacteria in repair the uranium polluted water

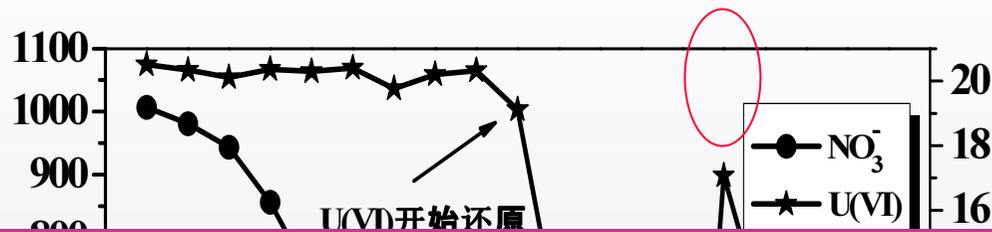
## Effect of the concentration of $\text{SO}_4^{2-}$ deoxidation precipitary the SBR

When the concentration of  $\text{SO}_4^{2+}$  was below 4000mg/L, it did not effect, but when the concentration of  $\text{SO}_4^{2+}$  above 5000mg/L, the deoxidize obviously existed inhibitory action about SBR to uranium, and it was related with the concentration of  $\text{SO}_4^{2+}$ .



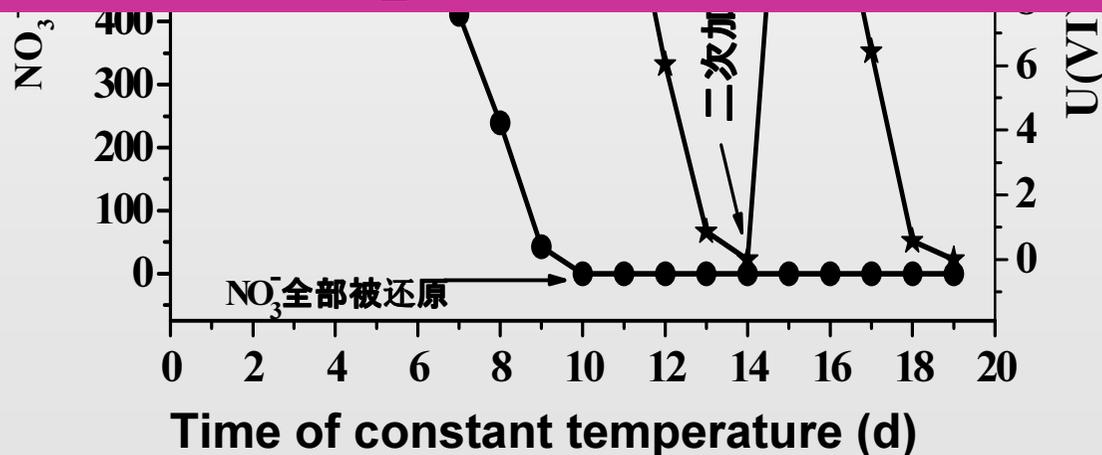
# The experiment results of sulfidogenic bacteria in repair the uranium polluted water

## (7) Influence of SRB Reduction and Precipitation U(VI) Caused by NO<sub>3</sub>'s Coexistence in Solution



Initial conditions: the concentration of NO<sub>3</sub><sup>-</sup> is 1006.9 mg/L, U 20.5 mg/L, before the 10th day

**Even there is only a little NO<sub>3</sub><sup>-</sup> in solution, the reduction process of U(VI) will be affected.**



In the 14th day, NO<sub>3</sub> whose concentration was 50 mg/L was added, and all the NO<sub>3</sub><sup>-</sup> was reduced 1 day later, the concentration of U rose to 17.1 mg/L, 4 days later, all the uranium was reduced, which indicated that the reduction process of U(VI) couldn't happen even only a little NO<sub>3</sub><sup>-</sup> exist in the solution

**The change of concentration when NO<sub>3</sub> and U(VI) coexist**



# Result and Discussion

**Influence of SRB's reduction ability on  $\text{SO}_4^{2-}$  caused by coexistence ions :  $\text{U}^{6+}$ ,  $\text{Fe}^{2+}$ ,  $\text{Cd}^{2+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Zn}^{2+}$  and  $\text{Pb}^{2+}$**

ELEMENTS	U	Cu	Cd	Zn	Pb
$\text{SO}_4^{2-}$ REMOVAL RATE					
5mg/L	83.2%	76.3%	83.9%	84.5%	86.2%
10mg/L	81.1%	77.1%	82.8%	81.6%	85.7%

**The toxicity sequence of heavy metal ions to SRB:  $\text{Cu}^{2+} > \text{U}^{6+} > \text{Cd}^{2+} > \text{Zn}^{2+} > \text{Pb}^{2+}$**

40mg/L	70.5%	62.7%	74.6%	70.4%	79.3%
50mg/L	66.8%	59.4%	67.7%	68.6%	78.5%



# The experiment results of the reduction of U(VI) by SRB in wastewater

Effect of coexisting ions ( $U^{6+}$ 、 $Cd^{2+}$ 、 $Cu^{2+}$ 、 $Zn^{2+}$ 、 $Pb^{2+}$ ) on reducing  $SO_4^{2-}$  of SRB



SRB could enzymatic and reduce U(VI) for insoluble U(VI), and the removal on U(VI) was 98~99% after 20 days.

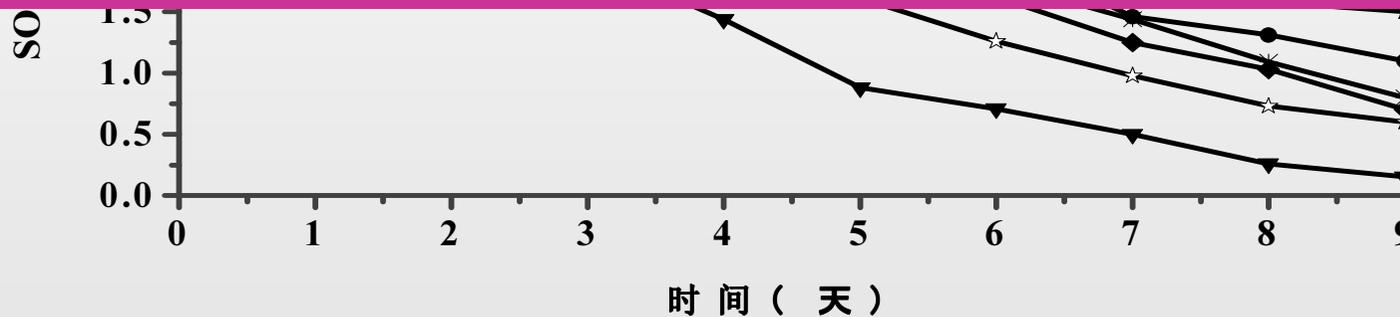


图 1、U、Cu、Cd、Zn和 Pb30mg/L对 SRB还原  $SO_4^{2-}$  的影响

Fig.1 Effect of the concentration of the coexisting ions ( $U^{6+}$ 、 $Cd^{2+}$ 、 $Cu^{2+}$ 、 $Zn^{2+}$ 、 $Pb^{2+}$ ) for 30mg/L.



# The experiment results of the reduction of U(VI) by SRB in wastewater

The removal on SRB reducing  $\text{SO}_4^{2-}$  was highest (95.8%), when the concentration of  $\text{Fe}^{2+}$  were 50~1500mg/L, the precipitation efficiency of FeS was 96.5~99%.

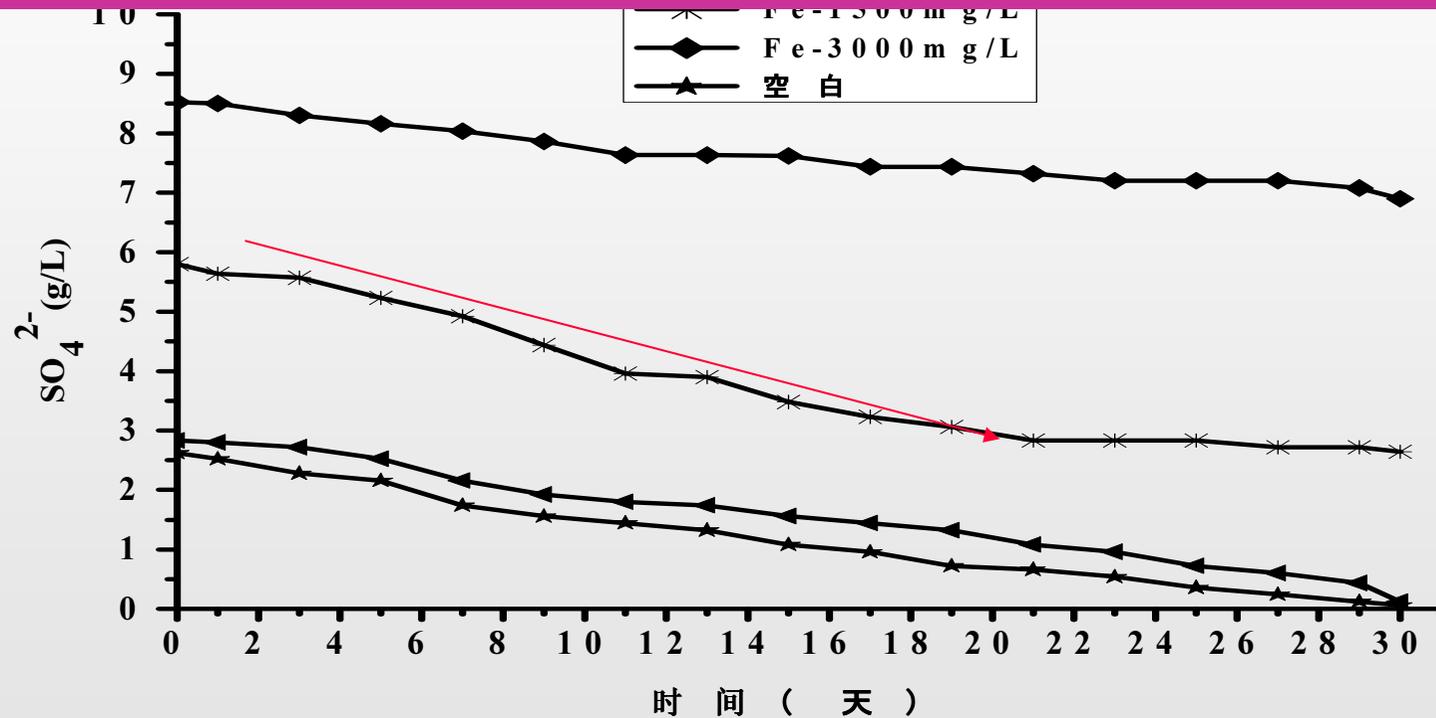


图 2 不同浓度的  $\text{Fe}^{2+}$  对 SRB 还原  $\text{SO}_4^{2-}$  的影响

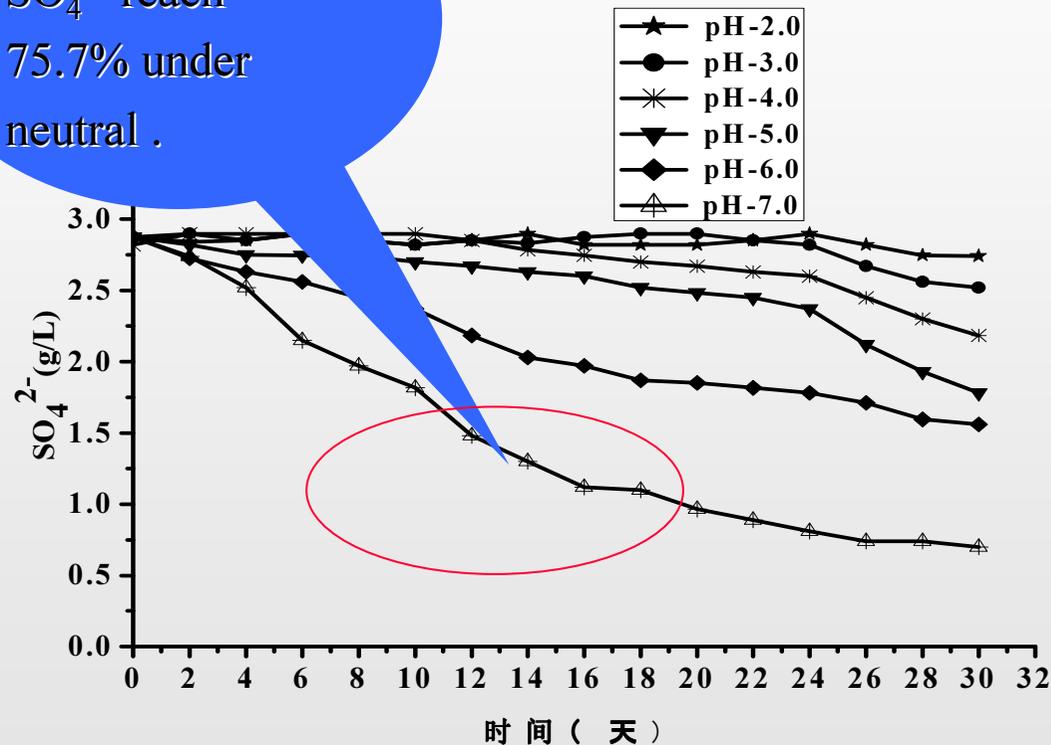
Effect of the different concentration on reduction of  $\text{SO}_4^{2-}$  by SRB.



# The experiment results of the reduction of U(VI) by SRB in wastewater

Effect of pH on reduction efficiency of  $\text{SO}_4^{2-}$  by SRB.

The removal of  $\text{SO}_4^{2-}$  reach 75.7% under neutral .

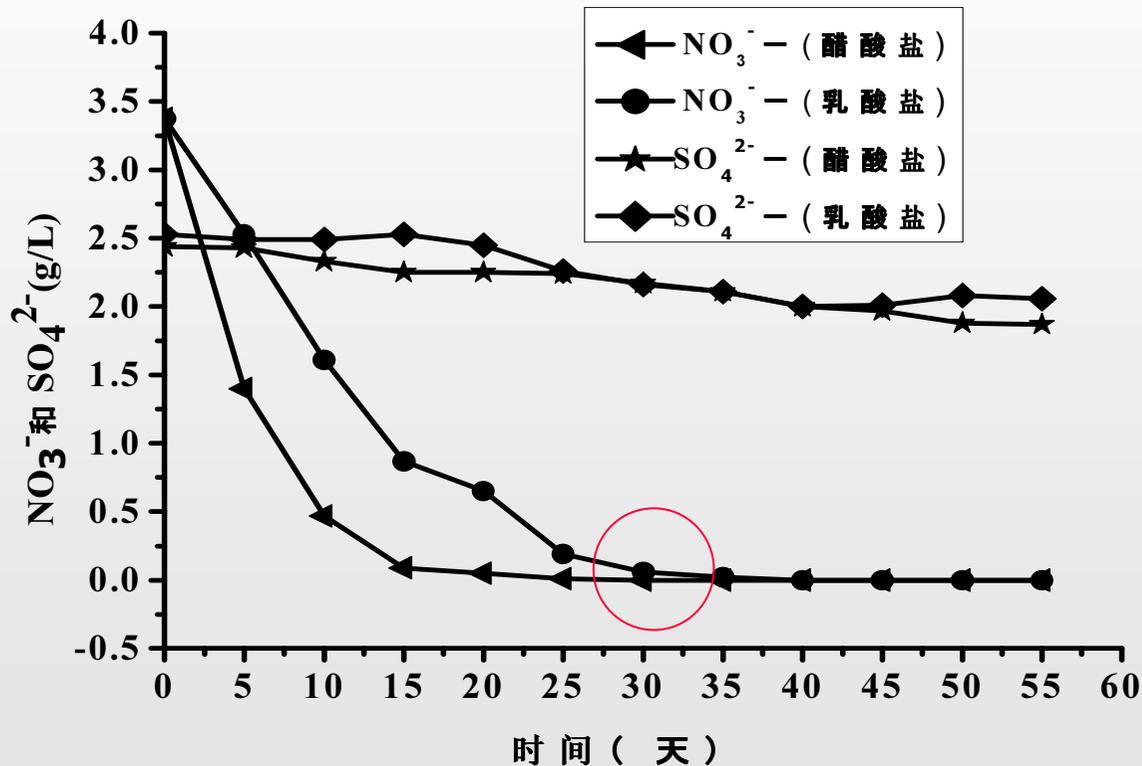


SRB had active in pH of 5.0 and 6.0, and the activity increased with increasing of pH. The removal rate of  $\text{SO}_4^{2-}$  also grew. The removal rate of  $\text{SO}_4^{2-}$  were respectively reached to 38.1% and 45.7% at 30 days. The max rate is 75.7% at pH of 5.0



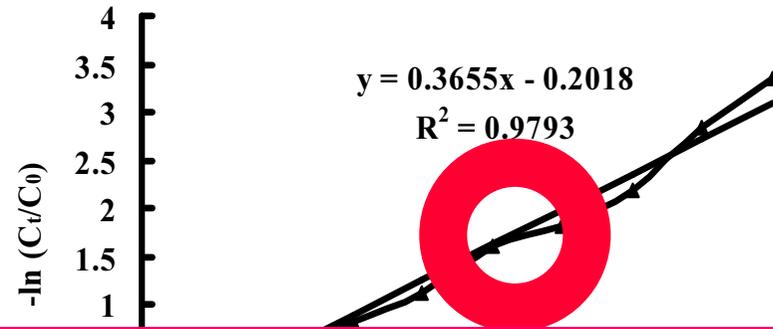
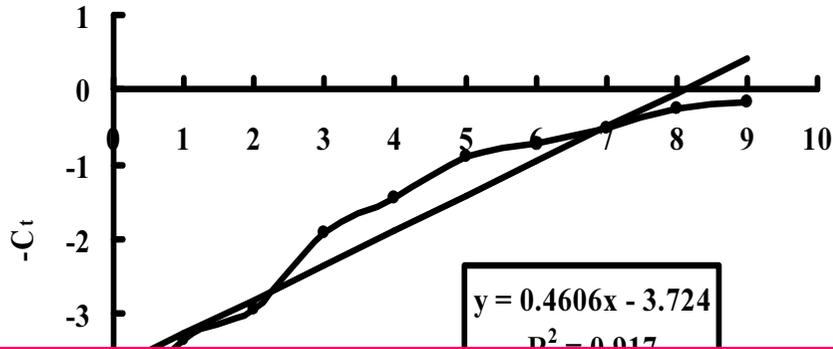
# The experiment results on reduction U(VI) by SRB wastewater

Effect of nitrate of high concentration on reduction efficiency of  $\text{SO}_4^{2-}$  by SRB.



The max removal rate of  $\text{NO}_3^-$  is 440mg/L·d, with carbon source of acetate. With carbon source of lactic acid, the rate obviously reduced. Prior to 30 days, denitrifying bacteria predominate on denitrification reaction. The reduction of  $\text{SO}_4^{2-}$  began after 30 days.





The reaction of SRB deoxidize sulfate radical comply with the first order chemical reaction kinetics,  $R^2=0.9793$

Fig.3 Fitting Chart of  $-C_t - t$

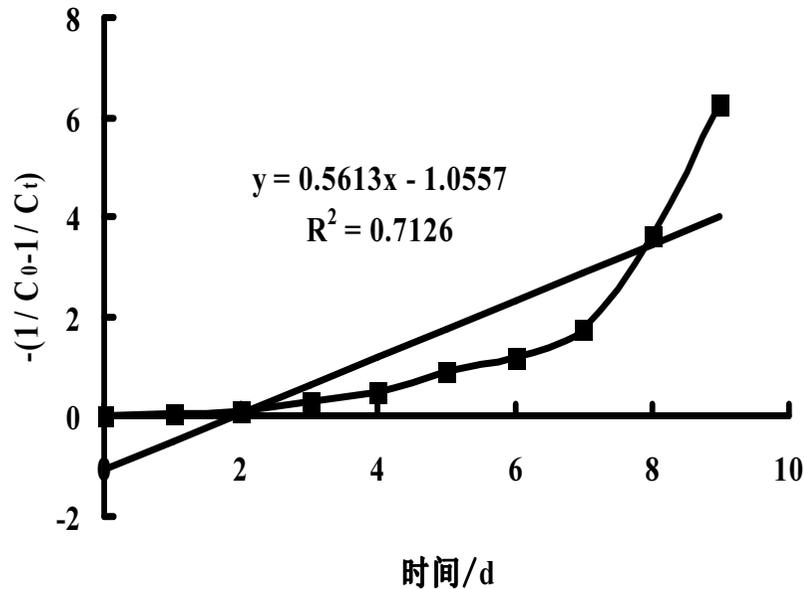


Fig.5 Fitting Chart of  $-(1/C_0 - 1/C_t) - t$

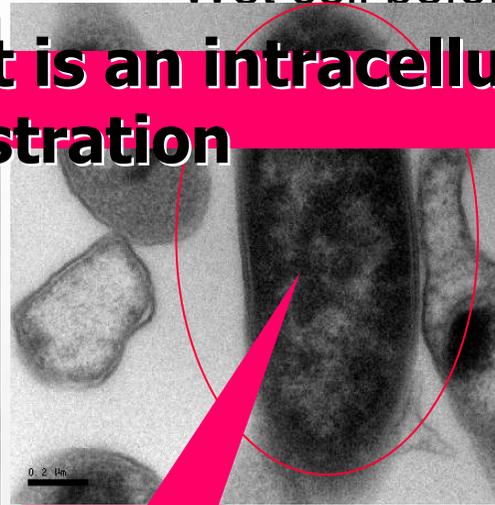
From the curve and the related coefficient of the fig, it can be seen that  $R^2=0.9793$  of the first order reaction, linear is better.



# The results of *Bacillus subtilis* adsorption of uranium by transmission electron microscope TEM

Wet cell before and after adsorption

**TEM analyses that is an intracellular sequestration**



(a) Before adsorption  
magnification:  $\times 0000$

- Transmission electron micrographs of uranium loaded cells revealed a dark opaque region throughout the cytoplasm indicating the intracellular sequestration of biosorbed metals the presence of accumulated radionuclides.
- It had better to use EDX analyses to identify the deposited elements.
- No significant metal accumulation in extracellular polymers.

A large number of black material

(b) After adsorption,  
magnification:  $\times 80000$

A large number of black material

Uranium has increased the permeability of cell membranes, once uranium ions through the membrane, the negative in cells through the chelate group, complexation, coordination etc, adsorbed the uranium acid-ion on cells.



# Summary

**In the treatment of radioactive wastewater with biotechnology, the concentration of nitrate is very important.** Denitrification reducing  $\text{NO}_3^-$  is the premise in uranium pollution control. Denitrifying bacteria could compete electron donor with SRB. Denitrification processes are more than sulfate-reducing activities of SRB in most cases. If the concentration of nitrate is up to 500 mg/L, sulfate-reducing activities will be inhibited.  $\text{NO}_3^-$  will impede bioreduction process of U(VI) entirely.

With the lower concentration of  $\text{NO}_3^-$ , there are bioreduction process. After U(VI) restored, readd  $\text{NO}_3^-$  will reverse the process of bioreduction of U(VI), the restore product of U(IV)/ $\text{UO}_2$  will oxidized and soluble in water.

**When the concentration of  $\text{SO}_4^{2-}$  is more than 5000 mg/L, the inhibition function will exist in bio-sedimentation of uranium, the inhibition increased with it. If it is less than 4000 mg/L, the effect is less.**

**There are synergy functions between SRB and other bacteria, Mixed SRB used to deal with the mixed acid-situ leaching of uranium water is better than a single strain. The removal rate of sulfate and uranium can be reached 93.5% and 75.5%. Mixed acid method for the in-situ leaching of uranium mining waste, the proposed mixed SRB bacteria and denitrifying bacteria.**



**When the concentration of U(VI) is 5~50 mg/L, it can be changed into insoluble U (IV) by SRB, the efficiency are as high as 98-99%. Uranium reduction process is catalyzed by SRB involved in negative charge of lactate with the electron transfer to U (VI) to form U (IV) / UO<sub>2</sub> enzymatic reduction. The activity of SRB in response to control by a variety of factors, pH affects the biological activity significantly, was positively correlated.**

**The results indicated that the concentration of U, Cu, Cd, Zn plasmas as high as 50 mg/L, SRB can grow, but be inhibited. With the increasing of concentration, the reduction rate of sulfate will decrease. The influence of Cu<sup>2+</sup> is the greatest on the SRB. Lower concentration of Cu<sup>2+</sup>, Zn<sup>2+</sup> are easy to form sulfide precipitation, there are less influence to PRB. But when the concentration of Cu<sup>2+</sup> 15mg/L and Zn<sup>2+</sup> 25mg/L, the restore process would be completely inhibited. When the range of concentration of Fe<sup>2+</sup> is 50~1500 mg/L, it can accelerate the reduction reaction of SRB. At the experiment range of pH, the max rate of SRB reduction happened at pH7, the removal rate of SO<sub>4</sub><sup>2-</sup> was 75.7%.**

**Using both ZVI and SRB to deal with in-situ leaching of uranium waste and SO<sub>4</sub><sup>2-</sup>, could enhance the efficiency up to 5-15%, it is indicated that between ZVI and SRB synergies, SRB is a reducing agent here and the catalyst as well.**



**It is very difficult to test with purified bacterial, due to the existence of mixed strain. The effects/results of biochemical methods dealing with wastewater of acid leaching of uranium may be better.**

**Using the physical and chemical properties of ZVI+ fluorspar, SRB-1 as catalytic agent, SRB-1 will synergism with ZVI, keep suitable environment for the microorganism, Such as adjusting pH or controlling the interfering ion. ZVI is excellent filling material of PRBs.**

**There are both the adsorption and the catalytic effects to SBR. The efficiency of cooperative processing ZVI may enhance 5~15%. You can adjust pH about 5.5 to control the concentration of nitrate ions. SBR could alive at weak acidic and radioactive conditions.**

**Optimal select microorganism and inorganic material. Carry on the pretreatment to the material or do some modifications for enhancing the performance of processing uranium.**



# The results of Biological isolation technology is stable

2005	influent		effluent		Removal rate %	remark
	PH	U(VI) /mg/L	U(VI) / mg/L	PH		
6. 11	2. 7	17. 80	0. 35	6. 78	98. 03	
6. 12.	2. 6	17. 42	0. 17	6. 85	99. 02	
6. 13.	2. 7	16. 91	0. 48	6. 70	97. 2	
6. 14.	3. 6	19. 61	0. 20	6. 78	99. 0	
6. 16	2. 7	20. 14	0. 22	7. 50	98. 9	
6. 18.	2. 9	21. 03	0. 53	7. 30	97. 6	
6. 20.	2. 8	19. 76	0. 75	6. 88	99. 2	
6. 24.	2. 6	67. 20	0. 09	7. 19	99. 8	
6. 28	2. 7	75. 10	0. 07	7. 21	99. 0	
7. 2.	2. 9	66. 30	0. 11	7. 12	99. 8	
7. 7.	3. 1	64. 70	0. 23	7. 03	99. 7	
7. 12.	3. 3	19. 78	0. 32	7. 13	98. 78	
7. 17.	3. 2	43. 2	0. 45	7. 15	98. 95	
7. 22.	3. 4	7. 61	0. 14	6. 98	98. 1	
7. 27.	2. 9	49. 1	0. 26	7. 03	99. 47	
8. 1.	3. 7	47. 5	0. 19	7. 14	99. 6	
8. 6	2. 9	32. 1	3. 20	5. 78	90. 0	
8. 11	3. 7	19. 1	1. 44	4. 89	92. 5	
8. 16	3. 9	17. 4	2. 11	5. 11	87. 87	
8. 21	4. 5	101. 4	0. 73	7. 18	99. 28	
8. 26	3. 7	108. 3	0. 35	6. 93	99. 7	

Removal rate is above 90%



## The result of biochemistry interception technology

Those are average results in 2006 from mines in Yunnan Province which is not beyond the criteria specific.

program	Before biochemistry interception		After biochemistry interception	
	effusion of tailing	Concentration of excretion	effusion of tailing	Concentration of excretion
pH	2.71	3.65	2.71	7.50
U/(mg/L)	16.21	1.46	16.21	0.003



# Conclusion and Suggestion 1

- In process of a separate ZVI reduction the solubility of hexavalent uranium reduction for insoluble tetravalent uranium, acidic conditions is benefit for removal of uranium. It is the first order reaction, corrosion product of iron and iron oxide can adsorpte U(VI).
- Adding artificially selected strain SPR-1, the hexavalent uranium is reduced to the difficult soluble tetravalent uranium, it is a bio-chemical reaction, and the removal rate could reach 40%.
- Most coexisting ions, such as  $U^{6+}$ ,  $Cu^{2+}$ ,  $Cd^{3+}$ ,  $Zn^{2+}$  and  $Pb^{2+}$  have inhibition on SRB, especially the  $Cu^{2+}$ . When the concentration of nitrate is more than 500mg/L or the concentration of  $SO_4^{2-}$  is more than 5000mg/L, the process of reducing will be inhibited completely. The concentration of inhibitory substances must be controlled effectively.
- Both the mixed flora of SRB and denitrifying bacteria should used when the uranium effluent from leaching process by the sulfuric acid method and nitric acid method at the same time.
- *Bacillus Subtilis* and *Citrobacter* are great amount of adsorption to uranium, more strong tolerance, more fast rate of adsorption that is more than 90% and easy to desorb. They are suit for recovering



# Conclusion and Suggestion 2

- uranium from the solution with lower concentration.
- The adsorption capability of bacteria to uranium have improved after treated *Citrobacter* by NaOH. At the zone of biological adsorption, the rates of dead thallus are better than the living ones. Carboxyl, amino and amide play an important role in the adsorption of uranium. The effect of using 4%PVA+1% sodium alginate as fixative to embed *Bacillus Subtilis* is better.
- The bench test and plant practice proved that the process of CITB is successful for uranium pollution control at the uranium tailings.
- Combined analysis of TEM and EDX, especially the specific part of thallus' biosorption, functional groups, create conditions for techniques of pretreatment and desorption agent, for improving the ability of adsorption capacity and adaptability.
- To isolate and purified in site bacteria, reform the bacteria. **establish** more advantage engineering strainod of acid resistant and radiation resistance.
- Study on stability genetic engineering bacteria;and ZVI and establish of biological, feasible models for directing the applying of bioabsorption method for industry.

